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RETURN RECEIPT REQUESTED

May 9, 2011

Illinois Environmental Protection Agency
Division of Air Pollution Control
Compliance Enforcement Section (#40)
P.O. Box 19276
Springfield, IL 62794

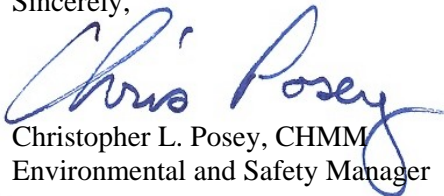
RE: Quarterly Compliance Report – 1st Calendar Quarter 2011
Adkins Energy, LLC
4350 West Galena Road
Lena, IL 61048
Site ID No: 177802AAA
FESOP Permit No: 03060057
DDGS Dryer/RTO Construction Permit No: 03040053
Standby Compression Ignition Construction Permit No: 07070030
Fermentation Construction Permit No: 07090050
RTO and Plant Capacity Increase Construction Permit No: 07110047
Corn Oil Extraction System Permit No: 07050002

Dear Sir/Madam:

Please find enclosed two (2) copies of the quarterly compliance report for the first calendar quarter (January through March) 2011.

If you have any questions or need any additional information, please do not hesitate to contact me at 815-369-9173.

Sincerely,


Christopher L. Posey, CHMM
Environmental and Safety Manager

Enclosure

cc: Mr. Dean Haden, IEPA – Peoria (with enclosure)
Certified Mail Number: 7010 1060 0001 2821 6036

Quarterly Compliance Report

**In Accordance with FESOP Permit Number 03060057
DDGS Dryer/RTO Construction Permit No. 03040053
Standby Compression Ignition Engine Construction Permit No. 07070030
Fermentation Scrubber Construction Permit No. 07090050
RTO and Plant Capacity Increase Construction Permit No. 07110047
Corn Oil Extraction System Permit No. 07050002**



**Adkins Energy, LLC
4350 West Galena Road
Lena, IL 61048
Site ID No: 177802AAA**

1st Quarter 2011

Submitted May 2011

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1.0 Introduction/Plant Wide Conditions

The purpose of this report is to satisfy the quarterly reporting requirements as identified in Special Condition 3.5.b of Adkins Energy LLC's FESOP Permit No: 03060057. This report covers the 1st calendar quarter (January through March) 2011. This report also satisfies the quarterly reporting requirements identified in the following construction permits:

- Special Condition 1.10.c) of the facility's DDGS Dryer/RTO Construction Permit No: 03040053;
- Special Condition 1.10 b) of the facility's Standby Compression Ignition Engine Construction Permit No: 07070030;
- Special Condition 1.10 a) and e) of the facility's Fermentation Scrubber Construction Permit No: 07090050;
- Special Condition 1.10 a) and e) and new limitations in Sections 2 and 3 of the facility's RTO and Plant Capacity Increase Construction Permit No: 07110047;
- Special Condition 1.10 a) of the facility's Corn Oil Extraction System Construction Permit No: 07050002.

There were no deviations from the requirements in Section 1.0 Plant Wide Conditions during this reporting period. Adkins Energy, LLC was in compliance with all plant-wide operating and production limitations identified in the applicable permits during the 1st calendar quarter 2011, as determined monthly based on a running total of twelve (12) months of data, pursuant to the permit.

2.0 Unit Specific Conditions

2.1 Boilers

There were no deviations from permit requirements for this equipment during this reporting period.

2.2 Gas Turbine

There were no deviations from permit requirements for this equipment during this reporting period.

2.3 Grain Receiving and Handling

There were no deviations from permit requirements for this equipment during this reporting period.

2.4 Fermentation

Modifications were made under a construction permit to route the fermentation exhaust gas through the RTO stack to allow for better dispersion. Table 11 shows the times that the fermentation scrubber vent stack was open to the atmosphere during the quarter, rather than venting to the RTO. These times do not constitute a deviation, unless identified in Table 10, which describes in detail the deviations during the quarter. Immediate notifications and excess emissions estimates were submitted as appropriate. As identified in Table 10, there were two deviations associated with the fermentation operations during the 1st quarter 2011, both of which were due to power outages. Deviation reports were submitted as required.

Two (2) additional construction permits associated with the fermentation operations were issued in 2007. One (1) was for the installation of a “new” fermentation scrubber, consisting of a combination of the body of the original scrubber that was installed with the plant and the scrubber packing of the current scrubber. The second construction permit was for the installation of a regenerative thermal oxidizer to control fermentation in place of the scrubber.

The RTO was installed downstream of the scrubber, allowing the scrubber to function primarily as a product recovery device, with the RTO controlling emissions from the fermentation process. To allow for maintenance and repair as well as unplanned outages of the RTO, the fermentation units are allowed to operate for up to 336 hours with the scrubber providing emission control. The RTO combustion temperature is shown in Figure 2 along with the Dryer RTO combustion temperature. Figures 6-8 show the temperatures recorded at the fermentation scrubber during the 1st quarter 2011, as well as the corresponding CIP tank level during that time period.

2.5 Distillation

Excess emissions from the distillation equipment as a result of the opening of the dryer emergency vent valve due to an unplanned dryer shutdown are identified in Section 2.6 Feed Drying and Handling.

As shown in Table 4, there were three (3) scrubber deviation events recorded during the quarter. Events are only considered a deviation event if the process scrubber is online at the time, as indicated in Table 6. Additionally, temperature deviations are not considered cause for excess emissions, regardless of whether the temperature deviation is a result of a CIP event, provided the scrubber is otherwise operating properly. Figures 9-11 show the temperatures recorded at the distillation scrubber during the 1st quarter 2011, as well as the corresponding CIP tank level during that period. Uncontrolled VOM and HAP emissions from the distillation process during actual events are documented in Table 5. Distillation process deviation emission rates are assumed to be equal to the uncontrolled distillation process emissions measured at the distillation scrubber inlet during the August 2003 scrubber compliance demonstration test. Dryer emissions are addressed in the feed drying section of this report.

2.6 Feed Drying and Handling

This quarterly report includes the following information as it relates to Feed Drying and Handling:

- Summary of Dryer/RTO Operations and Operating Rates
- Dryer/RTO Emissions
Dryer Deviation Emissions
Distillation Scrubber Deviation Emissions
- Dryer/RTO Deviations
- Other Dryer Feed Interruptions
- Dryer Operating Trend Data

Summary of RTO Operations

The calculated average dryer feed rate (wet cake plus syrup) averaged approximately 27.55 tons per hour (tph) during the quarter. Dryer natural gas consumption averaged 51.71 MMBtu/hr during the quarter.

Dryer Emissions

Table 1 also presents a summary of dryer/RTO emissions during the quarter. All dryer operating hours were multiplied by the hourly emission rates measured during the compliance demonstration test to determine normal process emissions. Short term hourly emissions rates are less than the permitted short-term emission limitations and the total quarterly emissions, projected to annual emissions are less than permitted annual emissions.

Deviation emissions occur when an unplanned dryer shutdown triggers the opening of the dryer emergency vent stack allowing uncontrolled emissions from the dryer to be vented directly to the atmosphere. The emergency vent stack opens automatically in response to a number of dryer operating conditions that, when exceeded, may represent a safety hazard to plant personnel and equipment. Unexpected events that result in the emergency vent valve opening results in uncontrolled emissions from the dryer and/or distillation process (distillation scrubber). These deviations are described as follows:

Dryer Emission Deviation Events: Table 2 identifies eight (8) events during the quarter where the dryer emergency vent valve was opened during dryer operation. The events totaled 8 hours and 43 minutes that the vent was opened. Emissions from these events are identified in Table 3.

Emissions are calculated using data presented on Tables 8 and 9. When the emergency vent valve is opened (and the valve allowing dryer exhaust to go to the RTO is closed), the wet feed is stopped and the dryer burner is driven to the low fire position and shut down over an approximately one (1) to three (3) minute period depending on the cause of the event. The dryer combustion air fan speed decreases in relation to the dryer burner gas valve position reducing the amount of combustion air entering the dryer. As a result, the dryer recirculation fan speed is also decreased, reducing the gas discharge rate through the emergency vent. Due to the lack of specific gas flow rate and emission rate measurements from a shutdown event, a number of conservative assumptions have been made to estimate uncontrolled dryer emissions. Each of the assumptions introduces a high bias to the estimated emissions.

Dryer VOC and HAP emissions are assumed to be related to dryer inlet temperatures. Data from dryer burner shutdowns shows that the dryer inlet temperature decreases from approximately 740°F normal operating temperature to approximately 250°F in about three (3) minutes. NO_x and CO emission decrease and cease with the shutdown of the dryer burner. The dryer inlet temperature continues to decrease to approximately 160°F (the temperature of the wet cake discharged from the centrifuges) in about fifteen (15) minutes. At this point, VOM and HAP emissions should be insignificant.

Table 8 shows that emissions during the first three (3) minutes of the shutdown event (time required to reduce dryer inlet temperature to 250°F) are assumed to be equal to the full uncontrolled emission rate (lb/min) measured at the RTO inlet during the compliance demonstration test. Over the next 12 minutes, the dryer inlet temperature decreases to approximately 160°F. During this period, dryer emissions are assumed to be equal to the

average of the uncontrolled emission rates at 740°F and projected emissions at 160°F. During the next 45 minutes of a shutdown event, the dryer inlet temperature continues to decrease. Emissions during this period are assumed to be equal to the projected emission rates at 160°F. When the dryer duct temperatures reduce to 130°F, final shutdown occurs where all fans are stopped, effectively ending the emissions event. The time required for temperatures to reach 130°F will vary based on the ambient temperatures, however, in any case, the time is not expected to exceed 90 minutes.

Assumed emissions rates from 61 to 90 minutes following a shutdown are assumed to be equal to the projected emission rates (lb/min) at 160°F reduced by the ratio of 5,000 / 44,500 acfm, which represents the reduction in gas flow through the dryer vent. The measured gas flow rate at the RTO inlet was approximately 44,500 acfm during the dryer compliance test. The dryer vent gas flow is anticipated to reduce to approximately 5,000 cfm by the time the dryer inlet temperature reaches 160°F.

Table 9 presents a summary of the total calculated emissions (lbs) from any dryer shutdown event ranging from 1 minute to 90 minutes. The values in Table 9 were used in Table 3 to estimate total dryer deviation emission from each event. This table will be used for estimating future dryer deviation emissions as well.

Distillation Scrubber Emission Deviations: Distillation scrubber emissions are also vented to the RTO for VOC control. During an unexpected dryer shutdown and the emergency vent opens, distillation process emissions continue to be directed toward the RTO, and therefore are discharged through the emergency vent stack for several minutes until plant operators manually close an isolation valve and start the distillation scrubber fan and water flow. Scrubber deviation emissions are estimated based on the number of minutes from opening of the emergency vent stack and a positive scrubber pressure drop (and positive water flow rate), indicating that gas is flowing through the scrubber, is recorded. The time required to transition distillation process gas flow from the RTO to the scrubber varies depending on the severity of the dryer shutdown conditions and immediate availability of operators to manually close the valve.

Dryer Deviations

The causes of the dryer deviations are shown in Table 2. The cause of each event is evaluated, and where possible, changes in operating procedures and/or dryer programming are made to reduce repeated shutdowns from a single cause. Where deviations are traced to monitors or sensors, each device is checked and replaced as may be necessary. Where no problems are found at the suspect sensors, dryer programming and operating procedures are evaluated.

Other Dryer Feed Interruptions

When other non-critical operating conditions trigger an alarm and shut down the dryer feed system, the emergency vent valve does not open and dryer exhaust continues to be directed to the RTO. There can be multiple interruptions in dryer feed that do not result in opening the dryer emergency vent and these events are not reported because there are no excess emissions. Typically non-critical dryer feed interruptions are quickly corrected and feed is resumed. However, during prolonged feed interruptions, the dryer burner eventually shuts down. During non-critical feed interruptions, the RTO continues to operate normally and distillation emissions continue to be treated in the RTO.

Each time the dryer burner must be re-started, National Fire Protection Association (NFPA) and insurance requirements dictate that the dryer must be purged with at least five (5) volumes of ambient air prior to attempting to light the burner. These same requirements prohibit ducting of the purge emissions to a combustion device (RTO). Therefore, each time the dryer burner must be restarted, the emergency vent valve is opened for a period of ten (10) minutes. Normally, by the time the burner can be restarted, 30 to 60 minutes have elapsed and estimated dryer emissions are negligible, and distillation process emissions are redirected to the distillation scrubber prior to attempting to restart the burner. These are not excess emissions associated with these events and they are not separately recorded.

Dryer Operating Trend Data

Table 6 identifies the total time that the distillation process emissions are directed to the distillation scrubber. This data is simply tracked to allow calculation of facility emissions because the distillation process emissions are included in the RTO emissions when being treated in the RTO, but must be counted separately when treated in the distillation scrubber.

Table 7 shows the total amount of time the centrifuges are exhausted directly to the atmosphere rather than being treated by the RTO. These events do not represent an emission deviation.

Trend charts for several dryer operating parameters are attached to this quarterly report to provide an indication of the various dryer/RTO operating conditions throughout the quarter. Additional data on any specific period can be provided upon request from the IEPA. The following trend data is provided:

- Figure 1 - Dryer Emergency Vent Valve Position: This chart shows the position of the dryer emergency vent valve. A value of 1.0 indicates that the vent is closed. A value of 0 indicates the vent is open to the atmosphere. Each indication of an open vent is listed in Tables 2 and 3 (in the event that it is caused by a deviation event) or in Table 6 (in the event that it is shut down due to a high demand for wet cake).
- Figure 2 – RTO Combustion Chamber Temperature (°F)

- Figure 3 – Cyclone Differential Pressure (inches water column)
- Figure 4 – Dryer Inlet and Outlet Temperature (°F)
- Figure 5 – Dryer Natural Gas Consumption (scfm)

2.7 Storage Tanks

There were no deviations from permit requirements for this equipment during this reporting period.

2.8 Loading Rack

There were no deviations from permit requirements resulting in excess emissions for this equipment during this reporting period.

2.9 Leaking Components

There were no deviations from permit requirements for this equipment during this reporting period. There were no leaks identified during the quarter. When necessary, prompt repair of leaks assures minimal emissions as a result of the leak.

2.10 Bio-Methanator

There were no deviations from permit requirements for this equipment during this reporting period.

2.11 Cooling Tower

There were no deviations from permit requirements for this equipment during this reporting period.

2.12 Roadway/Fugitive Dust

There were no deviations from permit requirements for this equipment during this reporting period.

2.13 Standby Stationary Compression Ignition Engine

There were no deviations from permit requirements for this equipment during this reporting period.

2.14 Corn Oil Extraction System

There were no deviations from permit requirements for this equipment during this reporting period.

3.0 Signature by Responsible Official

Authorized Representative Signature:

Todd Block, General Manager

Signature _____

Date _____

Phone: (815) 369-9173

TABLES

TABLE 1

1ST QUARTER 2011 DRYER SUMMARY

Table 1.
First Quarter 2011 Summary of DDGS Dryer Operation and Production
Permit No. 03030054 - Dryer/RTO Construction Permit
Adkins Energy LLC - Lena, Illinois

Parameter	Units	1st Quarter 2011	Jan-11	Feb-11	Mar-11	Comments
Calendar Days in Month	days	90	31	28	31	
Total Hours in Quarter	hrs	2,160	744	672	744	Total days x 24 hours/day.
Total Days Dryer Operated	days	90	31	28	31	Entire days where dryer is voluntarily down for market reasons are excluded.
Potential Dryer Hours	hrs	2,160	744	672	744	Operating days x 24 hours/day.
Actual Dryer Hours	hrs	2,109	726	653	730	Reported operating hours including feed interruptions (dryer shutdowns).
Approximate On-Line Percentage	%	97.6%	97.5%	97.2%	98.2%	Actual operating hours / potential operating hours.
Total NG Consumed	MMBtu	109,054	38,374	33,648	37,032	Measured natural gas consumption at dryer.
Average NG Consumption	MMBtu/hr	51.71	52.9	51.5	50.7	
DDGS Production (11.8% m)	tons	23,256	8,155	7,444	7,657	Calculated production confirmed by sales and inventory records.
Average DDGS Production	tons/hr	11.03	11.24	11.39	10.49	Calculated production / actual operating hours.
Average Wet Feed Rate (65.7% m)	tons/hr	27.55	28.1	28.5	26.2	Convert dry solids in DDGS produced to equivalent wet feed (wet cake plus syrup).
DDGS Transfer Conveyor	tons	23,256	8,155.4	7,443.7	7,657.2	Assumes amount produced is amount transferred to storage bldg.
Dryer Emergency Vent Open	hh:mm	08:43	02:57	03:44	02:02	Total time dryer emergency vent is open.
Dist Scrub Vented to Dryer Emergency Vent	hh:mm	00:08	00:00	00:05	00:03	Time distillation scrubber is vented to atmosphere through dryer emergency vent.
DDGS Loadout	tons	23,920	7,316.77	7,781.14	8,821.82	Amount sold.
DDGS inventory (end of month)	tons	312	1,814.28	1,476.82	312.20	Amount produced - amount sold.

First Quarter 2011
SUMMARY OF DRYER/RTO QUARTERLY EMISSIONS
Adkins Energy LLC - Lena, Illinois

Parameter	Units	Quarterly Process Emissions		Dryer Deviation Emissions		Total Dryer/RTO Emission		Distillation Scrubber Deviation Emissions		Permitted Dryer/RTO Emissions	
		avg lb/hr	tons/qtr	lb/qtr	tons/qtr	lb/qtr	tons/qtr	lb/qtr	tons/qtr	lb/hr	tpy
DDGS Transfer PM Emissions	lb/hr	0.03	0.003	-	-	6.64	0.003	-	-	0.08	0.35
DDGS Loadout PM Emissions	lb/hr	3.82	0.502	-	-	1,004.63	0.502	-	-	5.88	6.62
PM/PM10	lb/hr	2.66	2.805	12.07	0.006	5,622.01	2.811	-	-	7.50	32.85
Carbon Monoxide	lb/hr	1.47	1.550	120.01	0.060	3,220.24	1.610	-	-	9.50	41.61
Nitrogen Oxide	lb/hr	3.80	4.007	-	-	8,014.20	4.007	-	-	8.80	38.54
Sulfur Dioxide	lb/hr	0.20	0.211	-	-	421.80	0.211	-	-	7.50	32.85
Total VOM (M25A/MSF)	lb/hr	1.72	1.808	296.81	0.148	3,913.74	1.957	11.38	0.006	4.00	17.52
Acetaldehyde (HAP)	lb/hr	0.05	0.050	24.79	0.012	124.45	0.062	0.62	0.000	0.50	2.19
Acrolein (HAP)	lb/hr	0.00	0.000	0.14	0.000	0.71	0.000	-	-	1.45	6.35
Formaldehyde (HAP)	lb/hr	0.01	0.012	3.70	0.002	28.30	0.014	-	-	1.45	6.35
Methanol (HAP)	lb/hr	0.12	0.123	4.16	0.002	251.11	0.126	0.01	0.000	1.45	6.35
Total HAPs	lb/hr	0.18	0.186	32.79	0.016	404.57	0.202	-	-	2.20	9.64

Dryer Natural Gas Consumption and DDGS Production/Sales

Jan-11			Ending Inventory Dec. 31, 10				975.63
Day	Dryer Natural Gas Usage		DDGS Rate tph	Dryer Operation hrs	DDGS Produced ton	DDGS Sold tons	DDGS Inventory tons
	therms	MMBtu					
01/01/11	13,570	1,357	12.23	24.00	293.52		1,269.15
01/02/11	13,426	1,343	12.31	24.00	295.44		1,564.59
01/03/11	12,938	1,294	11.88	24.00	285.12	269.94	1,579.77
01/04/11	12,223	1,222	11.44	24.00	274.56	642.44	1,211.89
01/05/11	12,987	1,299	12.30	24.00	295.20	343.07	1,164.02
01/06/11	13,398	1,340	11.75	24.00	282.00	264.09	1,181.93
01/07/11	13,536	1,354	11.94	24.00	286.56	420.28	1,048.21
01/08/11	13,578	1,358	12.00	24.00	288.00		1,336.21
01/09/11	13,316	1,332	12.64	24.00	303.36		1,639.57
01/10/11	12,295	1,230	11.15	24.00	267.60	434.72	1,472.45
01/11/11	12,223	1,222	11.22	24.00	269.28	546.51	1,195.22
01/12/11	6,208	621	11.40	11.50	131.10	576.83	749.49
01/13/11	9,650	965	10.45	20.00	209.00	224.68	733.81
01/14/11	10,952	1,095	9.98	22.00	219.56	207.10	746.27
01/15/11	11,542	1,154	9.32	24.00	223.68		969.95
01/16/11	13,357	1,336	11.14	24.00	267.36		1,237.31
01/17/11	13,424	1,342	11.35	24.00	272.40	180.28	1,329.43
01/18/11	13,432	1,343	11.45	24.00	274.80	325.09	1,279.14
01/19/11	13,112	1,311	11.02	24.00	264.48	482.57	1,061.05
01/20/11	12,319	1,232	11.02	24.00	264.48	417.59	907.94
01/21/11	12,505	1,251	10.89	24.00	261.36	228.55	940.75
01/22/11	12,364	1,236	10.64	24.00	255.36		1,196.11
01/23/11	12,259	1,226	10.22	24.00	245.28		1,441.39
01/24/11	12,159	1,216	10.86	24.00	260.64	360.78	1,341.25
01/25/11	12,125	1,213	10.79	24.00	258.96	383.39	1,216.82
01/26/11	12,228	1,223	10.48	24.00	251.52	472.99	995.35
01/27/11	12,286	1,229	10.70	24.00	256.80	220.35	1,031.80
01/28/11	12,205	1,221	11.27	24.00	270.48	138.35	1,163.93
01/29/11	12,253	1,225	11.64	24.00	279.36		1,443.29
01/30/11	13,104	1,310	11.27	24.00	270.48		1,713.77
01/31/11	12,763	1,276	11.57	24.00	277.68	177.17	1,814.28
TOTALS	383,737	38,374	11.24	725.50	8,155.42	7,316.77	
Average		52.89		97.5%			

Dryer Natural Gas Consumption and DDGS Production/Sales

Feb-11			Ending Inventory Jan. 31,11				1,814.28
Day	Dryer Natural Gas Usage		DDGS Rate tph	Dryer Operation hrs	DDGS Produced ton	DDGS Sold tons	DDGS Inventory tons
	therms	MMBtu					
02/01/11	10,251	1,025	11.46	19.50	223.47	327.13	1,710.62
02/02/11	8,679	868	11.66	16.50	192.39		1,903.01
02/03/11	12,888	1,289	11.55	24.00	277.20	111.59	2,068.62
02/04/11	12,559	1,256	11.47	24.00	275.28	432.01	1,911.89
02/05/11	10,795	1,080	9.74	24.00	233.76		2,145.65
02/06/11	11,525	1,153	10.90	24.00	261.60		2,407.25
02/07/11	11,811	1,181	11.27	24.00	270.48	549.97	2,127.76
02/08/11	12,520	1,252	12.52	24.00	300.48	543.98	1,884.26
02/09/11	12,621	1,262	11.58	24.00	277.92	503.00	1,659.18
02/10/11	12,916	1,292	11.87	24.00	284.88	208.96	1,735.10
02/11/11	12,190	1,219	11.17	24.00	268.08	223.22	1,779.96
02/12/11	12,031	1,203	10.80	24.00	259.20		2,039.16
02/13/11	12,742	1,274	12.18	24.00	292.32		2,331.48
02/14/11	12,706	1,271	11.80	24.00	283.20	375.84	2,238.84
02/15/11	12,932	1,293	11.03	24.00	264.72	577.41	1,926.15
02/16/11	12,553	1,255	11.50	24.00	276.00	697.83	1,504.32
02/17/11	12,081	1,208	12.65	24.00	303.60	427.96	1,379.96
02/18/11	10,871	1,087	10.70	24.00	256.80	400.05	1,236.71
02/19/11	12,081	1,208	10.92	24.00	262.08		1,498.79
02/20/11	12,218	1,222	10.85	24.00	260.40		1,759.19
02/21/11	12,089	1,209	11.24	24.00	269.76	296.90	1,732.05
02/22/11	12,864	1,286	11.78	24.00	282.72	701.87	1,312.90
02/23/11	12,996	1,300	11.67	24.00	280.08	259.74	1,333.24
02/24/11	10,132	1,013	10.58	20.25	214.25	256.21	1,291.28
02/25/11	12,188	1,219	11.97	24.00	287.28	368.18	1,210.38
02/26/11	11,124	1,112	11.37	21.00	238.77		1,449.15
02/27/11	13,139	1,314	11.58	24.00	277.92		1,727.07
02/28/11	12,977	1,298	11.21	24.00	269.04	519.29	1,476.82
		-			-		1,476.82
		-			-		1,476.82
		-			-		1,476.82
TOTALS	336,479	33,648	11.39	653.25	7,443.68	7,781.14	
Average		51.51		87.8%			

Dryer Natural Gas Consumption and DDGS Production/Sales

Mar-11			Ending Inventory Feb 28-11				1,476.82
Day	Dryer Natural Gas Usage		DDGS Rate tph	Dryer Operation hrs	DDGS Produced ton	DDGS Sold tons	DDGS Inventory tons
	therms	MMBtu					
03/01/11	13,073	1,307	11.20	24.00	268.80	499.67	1,245.95
03/02/11	13,201	1,320	10.61	24.00	254.64	351.47	1,149.12
03/03/11	13,232	1,323	10.88	24.00	261.12	498.71	911.53
03/04/11	12,316	1,232	10.73	24.00	257.52	407.72	761.33
03/05/11	12,119	1,212	10.67	24.00	256.08	-	1,017.41
03/06/11	12,011	1,201	10.58	24.00	253.92	-	1,271.33
03/07/11	12,134	1,213	10.75	24.00	258.00	799.20	730.13
03/08/11	12,119	1,212	10.55	24.00	253.20	438.00	545.33
03/09/11	12,277	1,228	10.50	24.00	252.00	385.25	412.08
03/10/11	12,238	1,224	10.10	24.00	242.40	144.07	510.41
03/11/11	12,421	1,242	9.87	24.00	236.88	356.26	391.03
03/12/11	12,254	1,225	10.50	24.00	252.00	-	643.03
03/13/11	12,243	1,224	10.35	24.00	248.40	-	891.43
03/14/11	12,243	1,224	10.55	24.00	253.20	314.93	829.70
03/15/11	12,141	1,214	10.42	24.00	250.08	418.47	661.31
03/16/11	11,076	1,108	9.77	24.00	234.48	77.01	818.78
03/17/11	12,060	1,206	10.10	24.00	242.40	326.66	734.52
03/18/11	12,238	1,224	10.77	24.00	258.48	439.41	553.59
03/19/11	12,050	1,205	10.23	24.00	245.52	-	799.11
03/20/11	12,316	1,232	10.43	24.00	250.32	-	1,049.43
03/21/11	12,261	1,226	10.37	24.00	248.88	673.36	624.95
03/22/11	12,393	1,239	10.65	24.00	255.60	548.71	331.84
03/23/11	9,538	954	10.27	19.25	197.70	125.70	403.84
03/24/11	12,064	1,206	10.12	24.00	242.88	405.94	240.78
03/25/11	11,937	1,194	10.45	24.00	250.80	248.44	243.14
03/26/11	11,741	1,174	10.47	24.00	251.28	-	494.42
03/27/11	11,737	1,174	10.92	24.00	262.08	-	756.50
03/28/11	11,740	1,174	10.70	24.00	256.80	487.30	526.00
03/29/11	11,906	1,191	10.31	24.00	247.44	513.44	260.00
03/30/11	7,373	737	10.18	15.00	152.70	175.13	237.57
03/31/11	11,870	1,187	10.90	24.00	261.60	186.97	312.20
TOTALS	370,322	37,032	10.49	730.25	7,657.20	8,821.82	
Average		50.71		98.2%			

TABLE 2

DRYER VENT DEVIATION EVENTS

TABLE 3

**UNCONTROLLED DRYER
EMISSIONS TO ATMOSPHERE**

TABLE 4

PROCESS SCRUBBER DEVIATION LOG

TABLE 5

PROCESS SCRUBBER DEVIATION EMISSIONS

Table 5. Process Scrubber Deviation Emissions (uncontrolled emissions through dryer emergency vent)
1st Quarter 2011

Date	Start Time (hh:mm)	End Time (hh:mm)	Duration (hh:mm)	Total VOM (M25A-MSF) (lbs)	Acetaldehyde (lbs)	Acrolein (lb)	Formaldehyde (lbs)	Methanol (lbs)	Total HAPs (lbs)
02/18/11	10:55	10:58	00:03	4.27	0.23	0.00	0.00	0.00	0.23
02/26/11	12:53	12:55	00:02	2.84	0.15	0.00	0.00	0.00	0.16
03/16/11	09:45	09:48	00:03	4.27	0.23	0.00	0.00	0.00	0.23
Totals			00:08	11.38	0.62	0.00	0.00	0.01	0.62

Uncontrolled distillation scrubber emissions are equal to the uncontrolled (scrubber inlet) emissions measured during the August 2003 scrubber compliance demonstration tests. Emission are equal to the number of minutes times 1/60th of the measured scrubber inlet emissions. These emissions are discharged from the dryer emergency vent stack. After an unexpected dryer shutdown occurs, operators must physically close distillation emission manifold valve leading to the RTO, open the distillation emission manifold valve leading to the scrubber, turn on scrubber fan and turn on scrubber water flow.

TABLE 6

PROCESS SCRUBBER ON-LINE TIMES

TABLE 7

CENTRIFUGE EVENTS TO ATMOSPHERE

TABLE 8

EMISSION RATE DATA

Table 8.
Summary of Emission Rate Data Used for Quarterly Report for
Permit No. 03030054 - Dryer/RTO Construction Permit
Adkins Energy LLC - Lena, Illinois

Parameter	Units	Distillation Scrubber Compliance Test August 2003		Dryer / RTO Compliance Test August 2004		Uncontrolled Dryer Emissions (measured at RTO Inlet) Scaled to Dryer Inlet Temperature			Note A	Note B	Note C	Note D	Note E
		Scrubber Inlet	Scrubber Outlet	RTO Inlet	RTO Outlet	Inlet Temp at Shutdown	Inlet Temp at 3 min.	Inlet Temp at 15 min.	Estimated of Dryer Emergency Shutdown Emissions (lb/min)				
									For the first 3 min	for the next 12 min	for the next 45 min	for the next 30 min	after 90 min
Measured Emissions						742 °F	250 °F	160 °F	0 to 3 min	4 to 15 min	16 - 60 min	61 - 90 min	> 90 min
Particulate Matter	lb/hr	NA	NA	3.57	2.66	3.57	1.20	0.77	0.06	0.04	0.02	0.02	-
CO	lb/hr	NA	NA	50.38	1.47	50.38	16.97	10.86	0.84	0.51	0.18	-	-
NOx	lb/hr	NA	NA	NA	3.80								
SO2	lb/hr	NA	NA	NA	< 0.20								
Total VOM (M25A/MSF)	lb/hr	85.33	1.09	122.10	1.72	122.10	41.14	26.33	2.04	1.24	0.44	0.05	-
Acetaldehyde (HAP)	lb/hr	4.62	0.42	10.20	0.05	10.20	3.44	2.20	0.16997	0.10331	0.03665	0.00412	-
Acrolein (HAP)	lb/hr	-	-	0.06	< 0.0003	0.06	0.02	0.01	0.00096	0.00059	0.00021	0.00002	-
Formaldehyde (HAP)	lb/hr	-	-	1.52	< 0.01	1.52	0.51	0.33	0.02538	0.01543	0.00547	0.00061	-
Methanol (HAP)	lb/hr	< 0.06	< 0.00	1.71	< 0.12	1.71	0.58	0.37	0.02854	0.01735	0.00615	0.00069	-
Total HAPs		4.68	0.42	13.49	0.18	13.49	4.55	2.91	0.22485	0.13667	0.04848	0.00545	-

DDGS Material Handling PM Emissions			
DDGS Transfer PM Emissions	lb/ton	Based on .005 gr/cf from baghouse and 140 tpy rate.	0.000286
DDGS Loadout PM Emissions	lb/ton	Based on USEPA lb/ton uncontrolled emission factor.	0.042000

- A. During the first three minutes after burn shutdown temps drop from operating temp to approximately 250°F. Assume conservatively that emissions during first 3 minutes are equal to the full uncontrolled emission rate.
- B. Assume emissions during next 12 mins (minute 4 through 15) are the average of uncontrolled emissions at 742 and 160°F.
- C. Assume emissions for next 45 minutes are emissions at 160°F.
- D. After initiation of shutdown the dryer discharge flow rate will decrease to about 5000 cfm (s.thompson) as fan speeds are reduced. Emissions are assumed to be the emissions at 160°F x (5,000 cfm/44,500 cfm) which was the average RTO inlet flow rate measured during the compliance test (44,500 acfm).
- E. After 90 minutes with the burner off - emissions are negligible because dryer fans are off when duct temp is <130F.
- F. Temp Vs. Time relationship for dryer shutdown taken from dryer inlet temperature trend chart for the dryer shutdown on August 12, 2004 at 1:54 AM.

TABLE 9

ESTIMATED DRYER SHUTDOWN EMISSIONS

**Table 9. Estimated Dryer Shutdown Emissions
Adkins Energy LLC - Lena, Illinois**

Total Dryer shutdown emissions table for periods of time when dryer vents directly to atmosphere and burner shuts down.										
Duration Time (hh:mm)	PM/PM10 (lbs)	CO (lbs)	NOx (lbs)	SO2 (lbs)	Total VOM (M25A/MSF) (lbs)	Acetaldehyde (lbs)	Acrolein (lbs)	Formaldehyde (lbs)	Methanol (lbs)	Total HAPs (lbs)
00:01	0.06	0.84	-	-	2.04	0.17	0.00	0.03	0.03	0.22
00:02	0.12	1.68	-	-	4.07	0.34	0.00	0.05	0.06	0.45
00:03	0.18	2.52	-	-	6.11	0.51	0.00	0.08	0.09	0.67
00:04	0.21	3.03	-	-	7.34	0.61	0.00	0.09	0.10	0.81
00:05	0.25	3.54	-	-	8.58	0.72	0.00	0.11	0.12	0.95
00:06	0.29	4.05	-	-	9.82	0.82	0.00	0.12	0.14	1.08
00:07	0.32	4.56	-	-	11.05	0.92	0.01	0.14	0.15	1.22
00:08	0.36	5.07	-	-	12.29	1.03	0.01	0.15	0.17	1.36
00:09	0.40	5.58	-	-	13.53	1.13	0.01	0.17	0.19	1.49
00:10	0.43	6.09	-	-	14.76	1.23	0.01	0.18	0.21	1.63
00:11	0.47	6.60	-	-	16.00	1.34	0.01	0.20	0.22	1.77
00:12	0.50	7.11	-	-	17.24	1.44	0.01	0.21	0.24	1.90
00:13	0.54	7.62	-	-	18.47	1.54	0.01	0.23	0.26	2.04
00:14	0.58	8.13	-	-	19.71	1.65	0.01	0.25	0.28	2.18
00:15	0.61	8.64	-	-	20.95	1.75	0.01	0.26	0.29	2.31
00:16	0.63	8.82	-	-	21.39	1.79	0.01	0.27	0.30	2.36
00:17	0.65	9.00	-	-	21.83	1.82	0.01	0.27	0.31	2.41
00:18	0.67	9.19	-	-	22.26	1.86	0.01	0.28	0.31	2.46
00:19	0.68	9.37	-	-	22.70	1.90	0.01	0.28	0.32	2.51
00:20	0.70	9.55	-	-	23.14	1.93	0.01	0.29	0.32	2.56
00:21	0.72	9.73	-	-	23.58	1.97	0.01	0.29	0.33	2.61
00:22	0.74	9.91	-	-	24.02	2.01	0.01	0.30	0.34	2.65
00:23	0.76	10.09	-	-	24.46	2.04	0.01	0.31	0.34	2.70
00:24	0.77	10.27	-	-	24.90	2.08	0.01	0.31	0.35	2.75
00:25	0.79	10.45	-	-	25.34	2.12	0.01	0.32	0.36	2.80
00:26	0.81	10.63	-	-	25.77	2.15	0.01	0.32	0.36	2.85
00:27	0.83	10.82	-	-	26.21	2.19	0.01	0.33	0.37	2.90
00:28	0.85	11.00	-	-	26.65	2.23	0.01	0.33	0.37	2.94
00:29	0.86	11.18	-	-	27.09	2.26	0.01	0.34	0.38	2.99
00:30	0.88	11.36	-	-	27.53	2.30	0.01	0.34	0.39	3.04
00:31	0.90	11.54	-	-	27.97	2.34	0.01	0.35	0.39	3.09
00:32	0.92	11.72	-	-	28.41	2.37	0.01	0.35	0.40	3.14
00:33	0.93	11.90	-	-	28.85	2.41	0.01	0.36	0.40	3.19
00:34	0.95	12.08	-	-	29.29	2.45	0.01	0.37	0.41	3.24
00:35	0.97	12.26	-	-	29.72	2.48	0.01	0.37	0.42	3.28
00:36	0.99	12.44	-	-	30.16	2.52	0.01	0.38	0.42	3.33
00:37	1.01	12.63	-	-	30.60	2.56	0.01	0.38	0.43	3.38
00:38	1.02	12.81	-	-	31.04	2.59	0.01	0.39	0.44	3.43
00:39	1.04	12.99	-	-	31.48	2.63	0.01	0.39	0.44	3.48
00:40	1.06	13.17	-	-	31.92	2.67	0.02	0.40	0.45	3.53
00:41	1.08	13.35	-	-	32.36	2.70	0.02	0.40	0.45	3.58
00:42	1.10	13.53	-	-	32.80	2.74	0.02	0.41	0.46	3.62
00:43	1.11	13.71	-	-	33.23	2.78	0.02	0.41	0.47	3.67
00:44	1.13	13.89	-	-	33.67	2.81	0.02	0.42	0.47	3.72
00:45	1.15	14.07	-	-	34.11	2.85	0.02	0.43	0.48	3.77
00:46	1.17	14.25	-	-	34.55	2.89	0.02	0.43	0.48	3.82

**Table 9. Estimated Dryer Shutdown Emissions
Adkins Energy LLC - Lena, Illinois**

Total Dryer shutdown emissions table for periods of time when dryer vents directly to atmosphere and burner shuts down.										
Duration Time (hh:mm)	PM/PM10 (lbs)	CO (lbs)	NOx (lbs)	SO2 (lbs)	Total VOM (M25A/MSF) (lbs)	Acetaldehyde (lbs)	Acrolein (lbs)	Formaldehyde (lbs)	Methanol (lbs)	Total HAPs (lbs)
00:47	1.18	14.44	-	-	34.99	2.92	0.02	0.44	0.49	3.87
00:48	1.20	14.62	-	-	35.43	2.96	0.02	0.44	0.50	3.91
00:49	1.22	14.80	-	-	35.87	3.00	0.02	0.45	0.50	3.96
00:50	1.24	14.98	-	-	36.31	3.03	0.02	0.45	0.51	4.01
00:51	1.26	15.16	-	-	36.75	3.07	0.02	0.46	0.52	4.06
00:52	1.27	15.34	-	-	37.18	3.11	0.02	0.46	0.52	4.11
00:53	1.29	15.52	-	-	37.62	3.14	0.02	0.47	0.53	4.16
00:54	1.31	15.70	-	-	38.06	3.18	0.02	0.47	0.53	4.21
00:55	1.33	15.88	-	-	38.50	3.22	0.02	0.48	0.54	4.25
00:56	1.35	16.07	-	-	38.94	3.25	0.02	0.49	0.55	4.30
00:57	1.36	16.25	-	-	39.38	3.29	0.02	0.49	0.55	4.35
00:58	1.38	16.43	-	-	39.82	3.33	0.02	0.50	0.56	4.40
00:59	1.40	16.61	-	-	40.26	3.36	0.02	0.50	0.56	4.45
01:00	1.42	16.79	-	-	40.69	3.40	0.02	0.51	0.57	4.50
01:01	1.43	16.79	-	-	40.74	3.40	0.02	0.51	0.57	4.50
01:02	1.45	16.79	-	-	40.79	3.41	0.02	0.51	0.57	4.51
01:03	1.47	16.79	-	-	40.84	3.41	0.02	0.51	0.57	4.51
01:04	1.49	16.79	-	-	40.89	3.42	0.02	0.51	0.57	4.52
01:05	1.51	16.79	-	-	40.94	3.42	0.02	0.51	0.57	4.52
01:06	1.52	16.79	-	-	40.99	3.42	0.02	0.51	0.57	4.53
01:07	1.54	16.79	-	-	41.04	3.43	0.02	0.51	0.58	4.53
01:08	1.56	16.79	-	-	41.09	3.43	0.02	0.51	0.58	4.54
01:09	1.58	16.79	-	-	41.14	3.44	0.02	0.51	0.58	4.55
01:10	1.60	16.79	-	-	41.19	3.44	0.02	0.51	0.58	4.55
01:11	1.61	16.79	-	-	41.24	3.44	0.02	0.51	0.58	4.56
01:12	1.63	16.79	-	-	41.29	3.45	0.02	0.51	0.58	4.56
01:13	1.65	16.79	-	-	41.34	3.45	0.02	0.52	0.58	4.57
01:14	1.67	16.79	-	-	41.38	3.46	0.02	0.52	0.58	4.57
01:15	1.68	16.79	-	-	41.43	3.46	0.02	0.52	0.58	4.58
01:16	1.70	16.79	-	-	41.48	3.46	0.02	0.52	0.58	4.58
01:17	1.72	16.79	-	-	41.53	3.47	0.02	0.52	0.58	4.59
01:18	1.74	16.79	-	-	41.58	3.47	0.02	0.52	0.58	4.59
01:19	1.76	16.79	-	-	41.63	3.48	0.02	0.52	0.58	4.60
01:20	1.77	16.79	-	-	41.68	3.48	0.02	0.52	0.58	4.61
01:21	1.79	16.79	-	-	41.73	3.49	0.02	0.52	0.59	4.61
01:22	1.81	16.79	-	-	41.78	3.49	0.02	0.52	0.59	4.62
01:23	1.83	16.79	-	-	41.83	3.49	0.02	0.52	0.59	4.62
01:24	1.85	16.79	-	-	41.88	3.50	0.02	0.52	0.59	4.63
01:25	1.86	16.79	-	-	41.93	3.50	0.02	0.52	0.59	4.63
01:26	1.88	16.79	-	-	41.98	3.51	0.02	0.52	0.59	4.64
01:27	1.90	16.79	-	-	42.03	3.51	0.02	0.52	0.59	4.64
01:28	1.92	16.79	-	-	42.08	3.51	0.02	0.52	0.59	4.65
01:29	1.93	16.79	-	-	42.12	3.52	0.02	0.53	0.59	4.65
01:30	1.95	16.79	-	-	42.17	3.52	0.02	0.53	0.59	4.66

TABLE 10
FERMENTATION (CO₂) SCRUBBER
DEVIATION LOG

TABLE 11

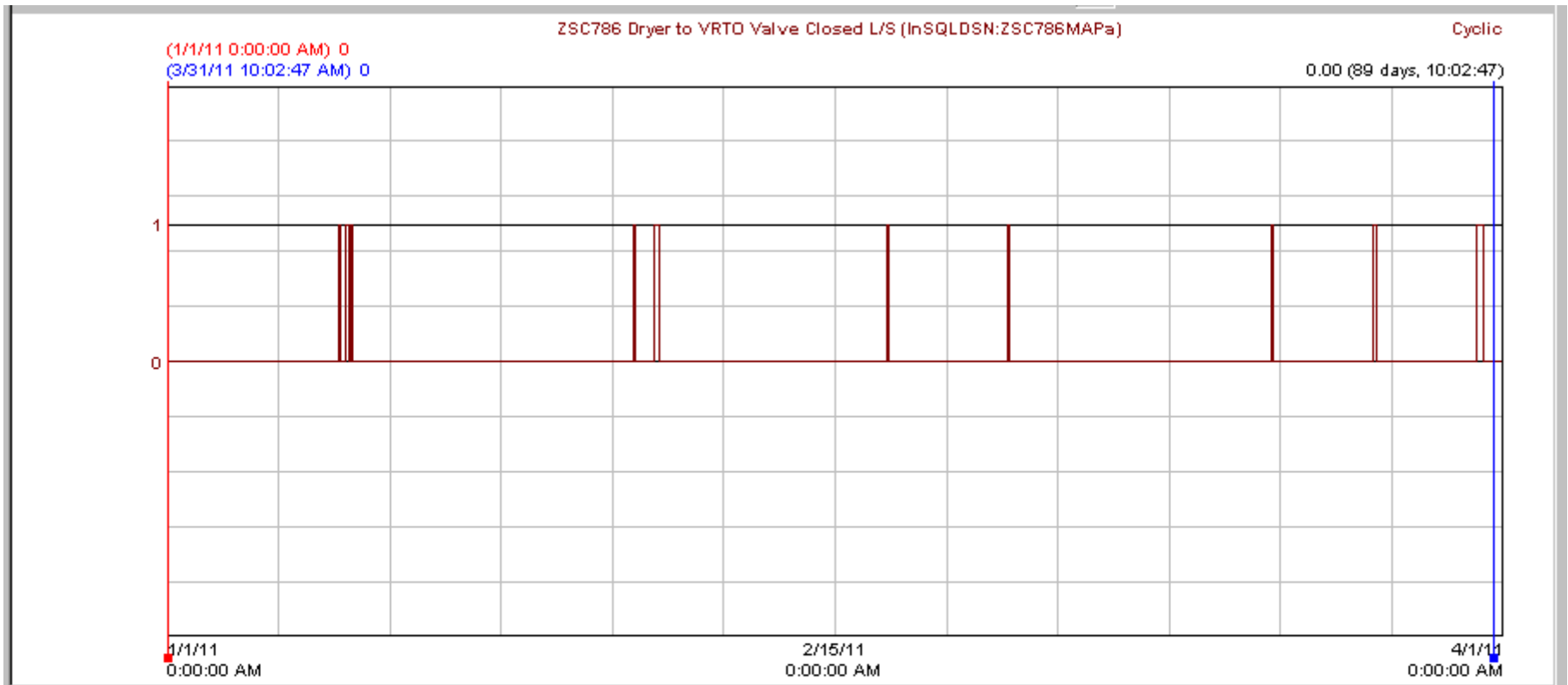
**FERMENTATION (CO₂) SCRUBBER
VENT STACK OPEN**

FIGURES

FIGURE 1

**DRYER EMERGENCY VENT VALVE POSITION
FIRST QUARTER 2011**

**Figure 1. Dryer Emergency Vent Valve Position
First Quarter 2011
Adkins Energy LLC – Lena, Illinois**

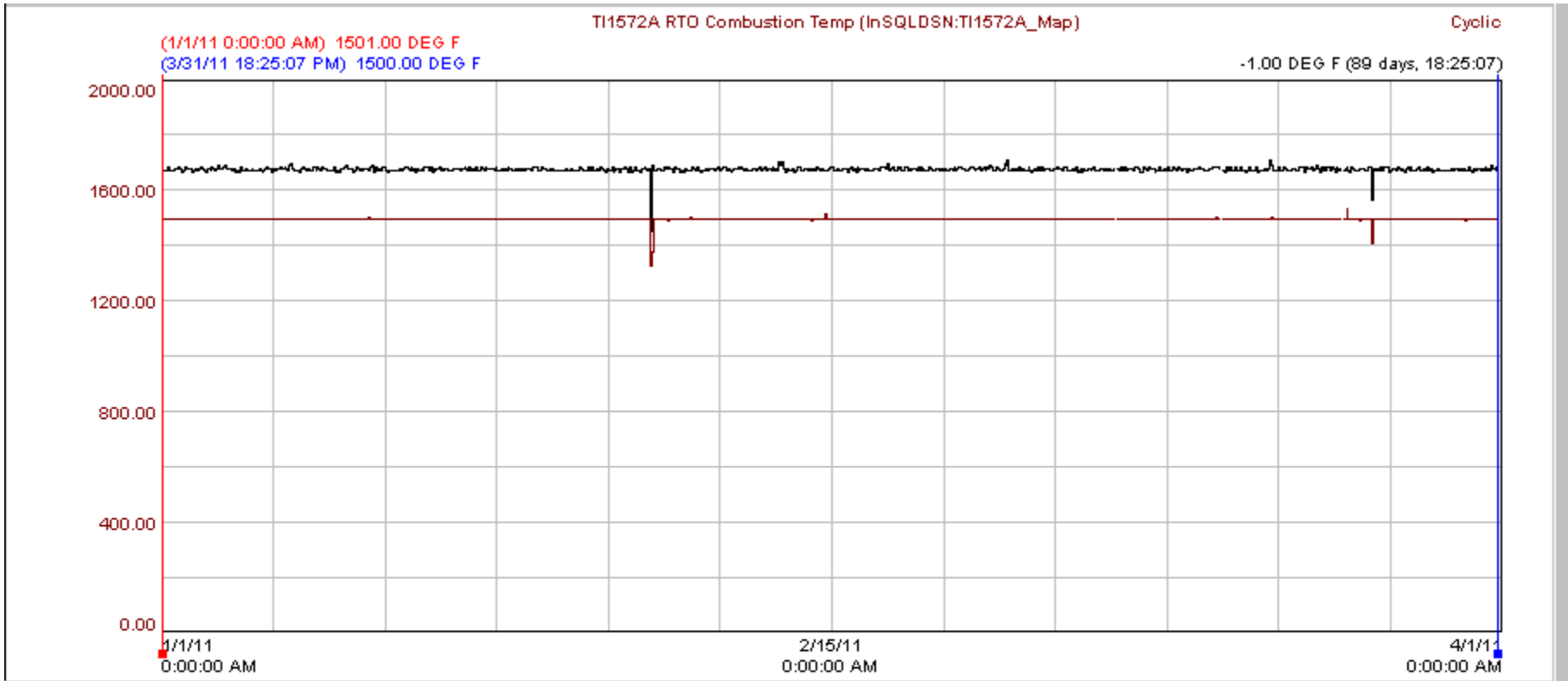


Typ	Tagname	Vis	Server	Description	Color	Units	Precision	Format	IOAddress	MinRaw	MaxRaw
└─┘	ZSC785MAPa	x	InSQLDSN	ZSC785 Dryer Vent Valve Closed L/S	=====	0 1	2	Decimal	\\HIST1\APACSIADK01IADK		
└─┘	ZSC786MAPa	x	InSQLDSN	ZSC786 Dryer to VRTO Valve Closed L/S	=====	0 1	2	Decimal	\\HIST1\APACSIADK01IADK		

FIGURE 2

RTO COMBUSTION CHAMBER TEMPERATURE (°F)

**Figure 2. RTO Combustion Chamber Temperature (°F)
 First Quarter 2011
 Adkins Energy LLC – Lena, Illinois**



Typ	Tagname	Vis	Server	Description	Color	Units	Precisior	Format	IOAddress	MinRaw	MaxRaw
~	TI1472a	x	InSQLDSN	RTO Combustion Temperature	====	°F	2	Decimal	\\HIST1\APACS\ADK01\ADK	0	2000
~	TI1572A_Map	x	InSQLDSN	TI1572A RTO Combustion Temp	====	DEG F	2	Decimal	\\HIST1\APACS\ADK01\ADK	0	9999

FIGURE 3

**CYCLONE DIFFERENTIAL PRESSURE
(INCHES IN WATER COLUMN)**

**Figure 3. Dryer Cyclone Differential Pressure (in. WC)
 First Quarter 2011
 Adkins Energy LLC – Lena, Illinois**

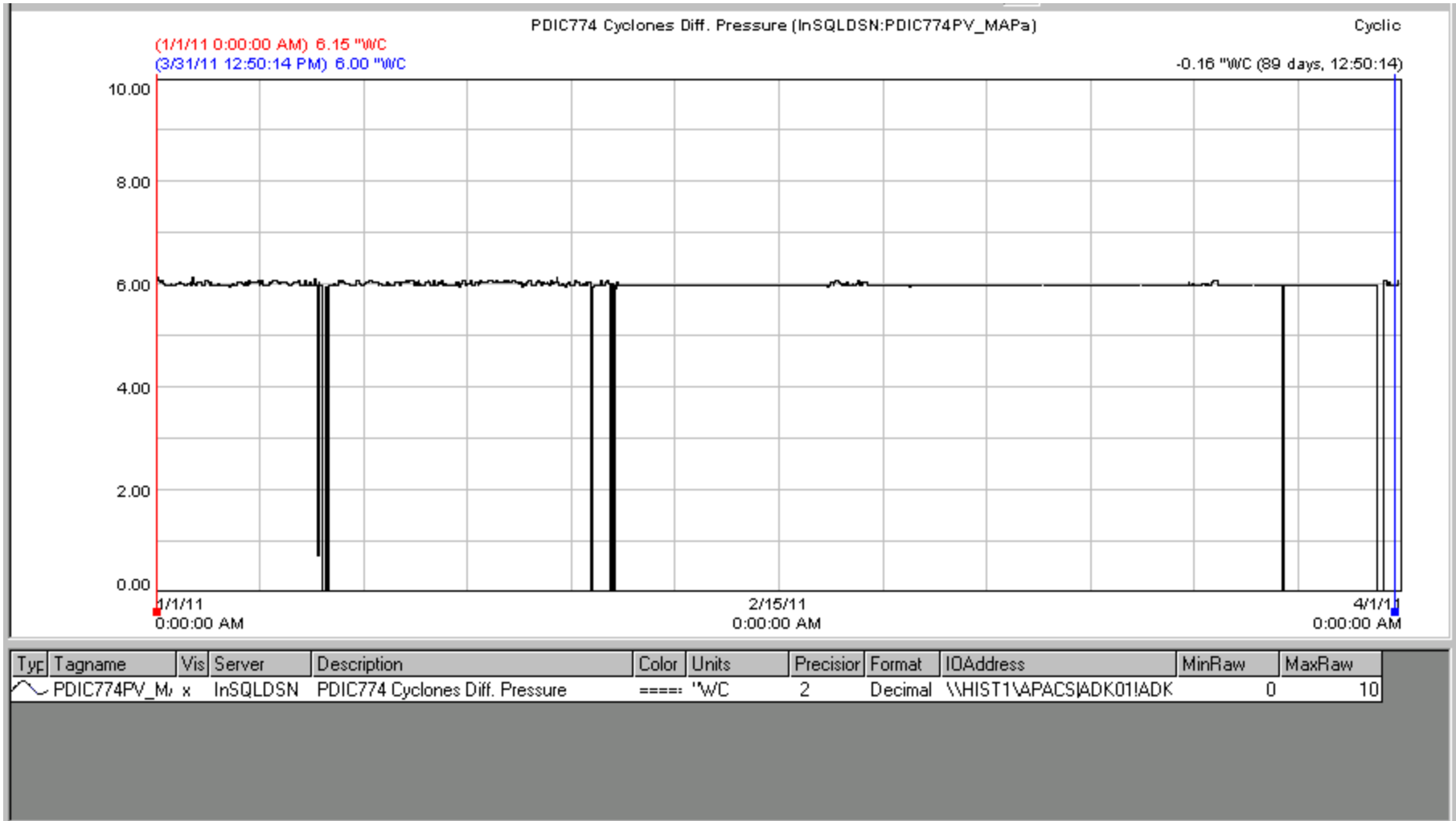


FIGURE 4

DRYER INLET AND OUTLET TEMPERATURE (°F)

**Figure 4. Dryer Inlet and Outlet Temperature (°F)
 First Quarter 2011
 Adkins Energy LLC – Lena, Illinois**

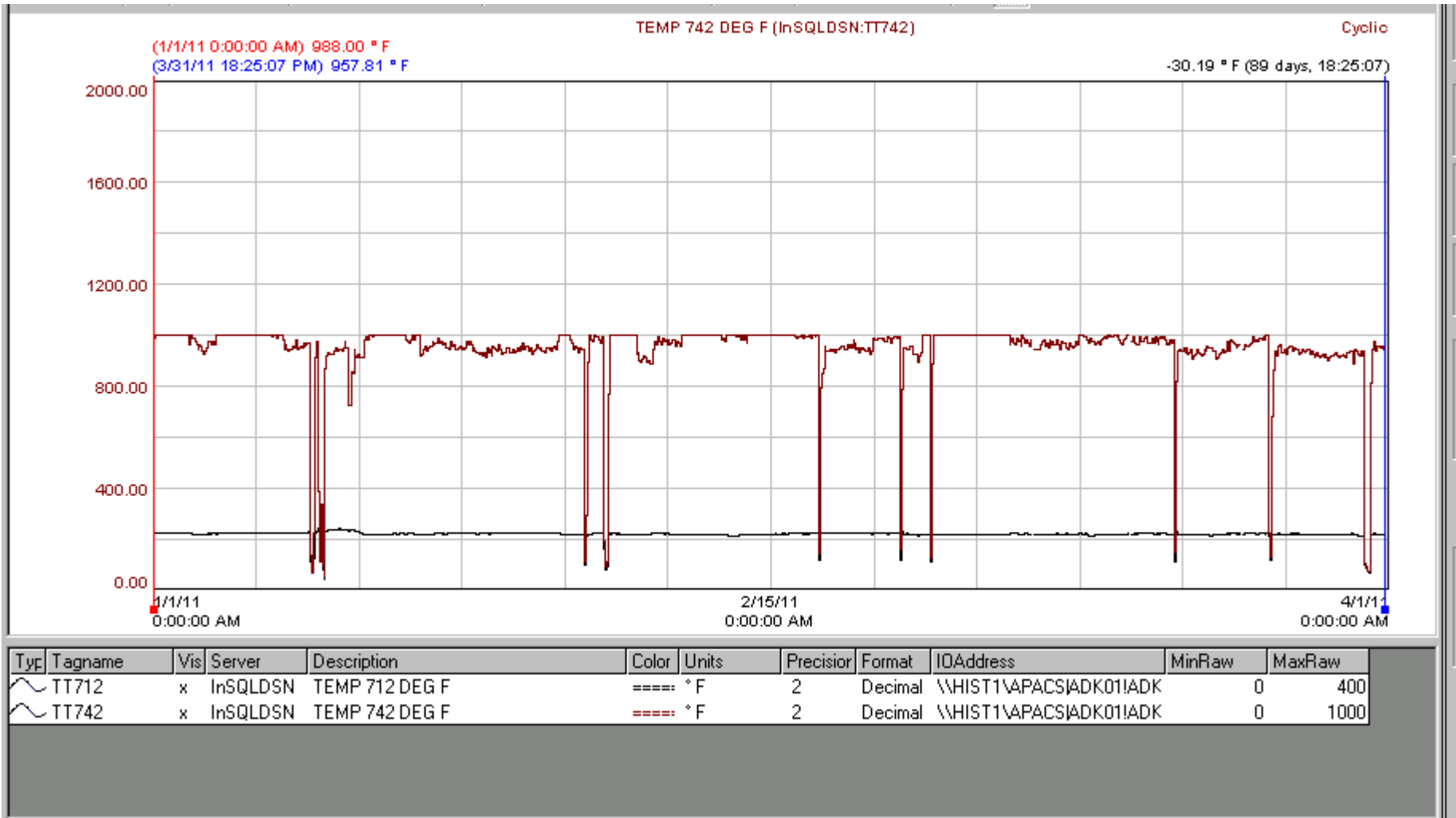


FIGURE 5

DRYER NATURAL GAS CONSUMPTION (SCFM)

**Figure 5. Dryer Natural Gas Consumption (cfm)
 First Quarter 2011
 Adkins Energy LLC – Lena, Illinois**

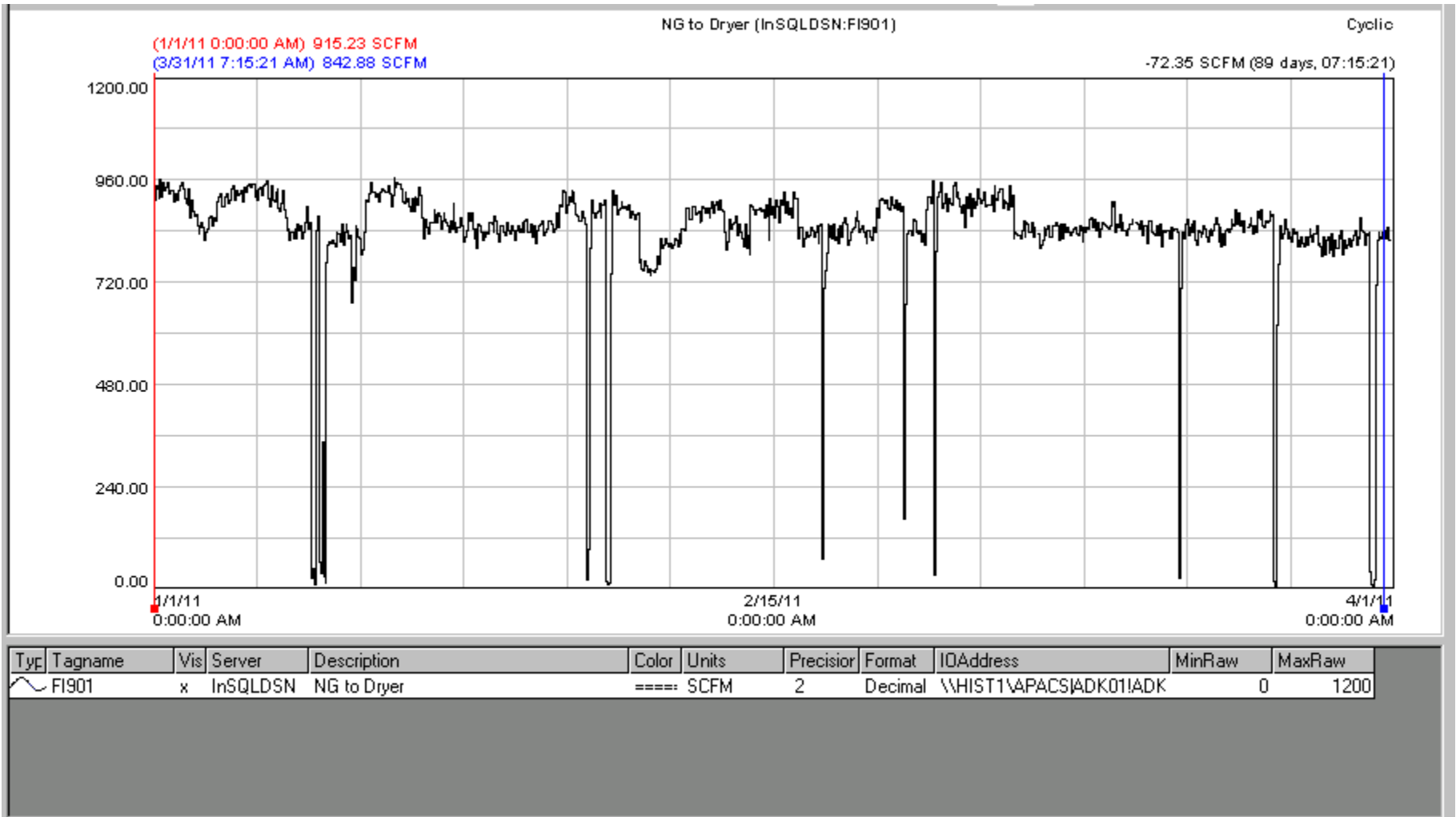


FIGURE 6

**FERMENTATION SCRUBBER TEMPERATURE
JANUARY 2011**

**Figure 6. Fermentation Scrubber Temperature (cfm)
January 2011
Adkins Energy LLC – Lena, Illinois**

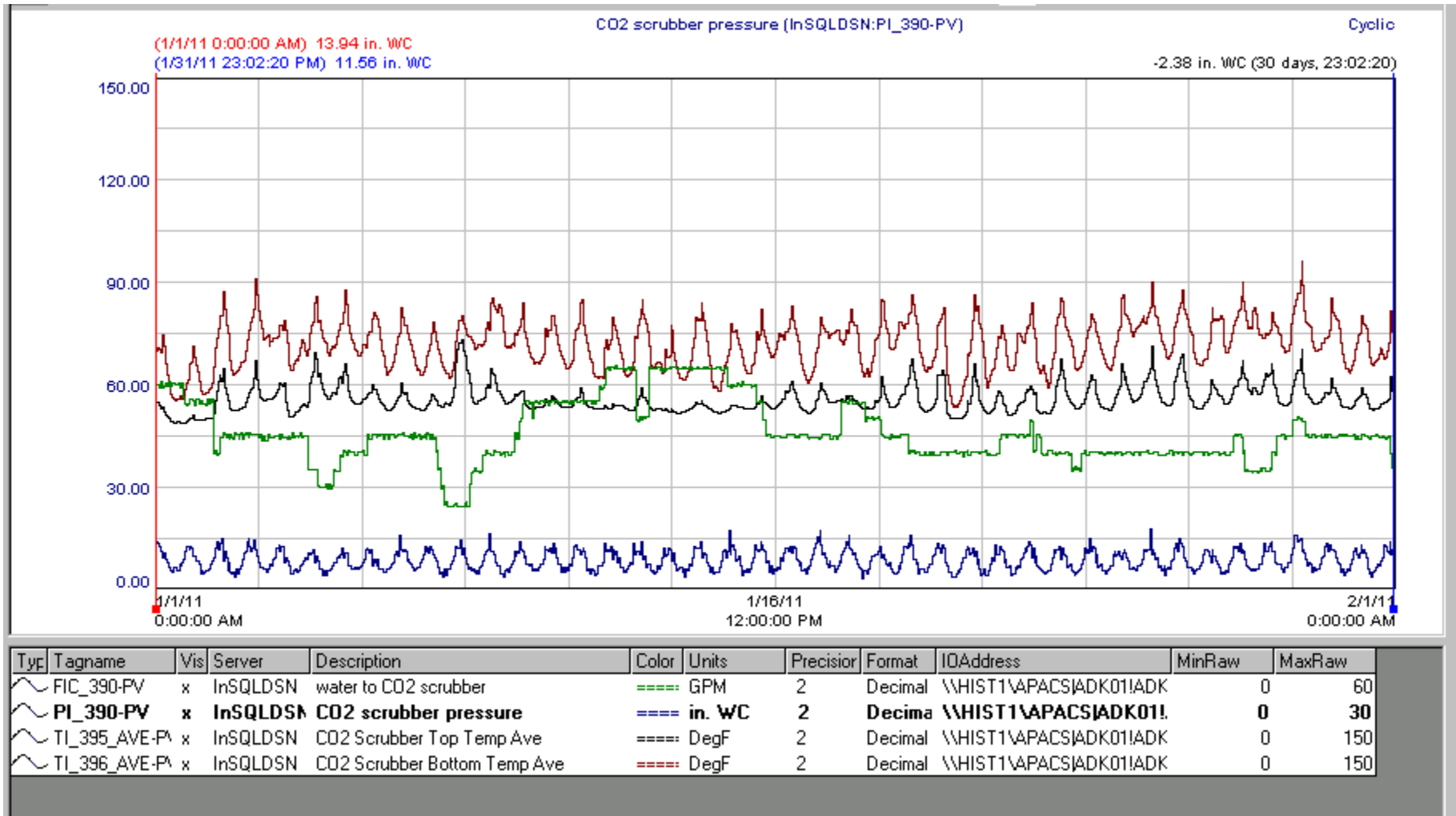


FIGURE 7

**FERMENTATION SCRUBBER TEMPERATURE
FEBRUARY 2011**

**Figure 7. Fermentation Scrubber Temperature
February 2011
Adkins Energy LLC – Lena, Illinois**

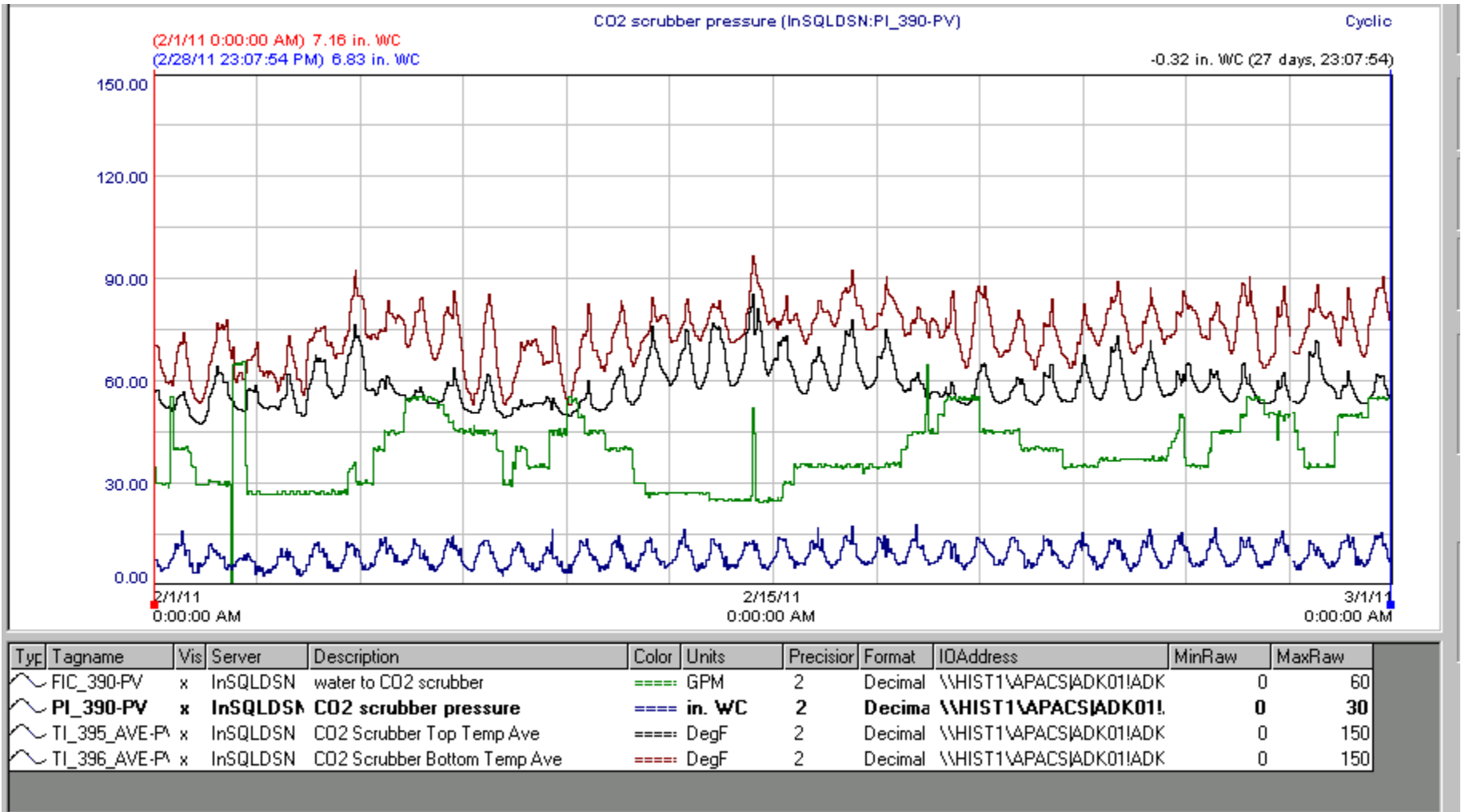


FIGURE 8

**FERMENTATION SCRUBBER TEMPERATURE
MARCH 2011**

**Figure 8. Fermentation Scrubber Temperature
March 2011
Adkins Energy LLC – Lena, Illinois**

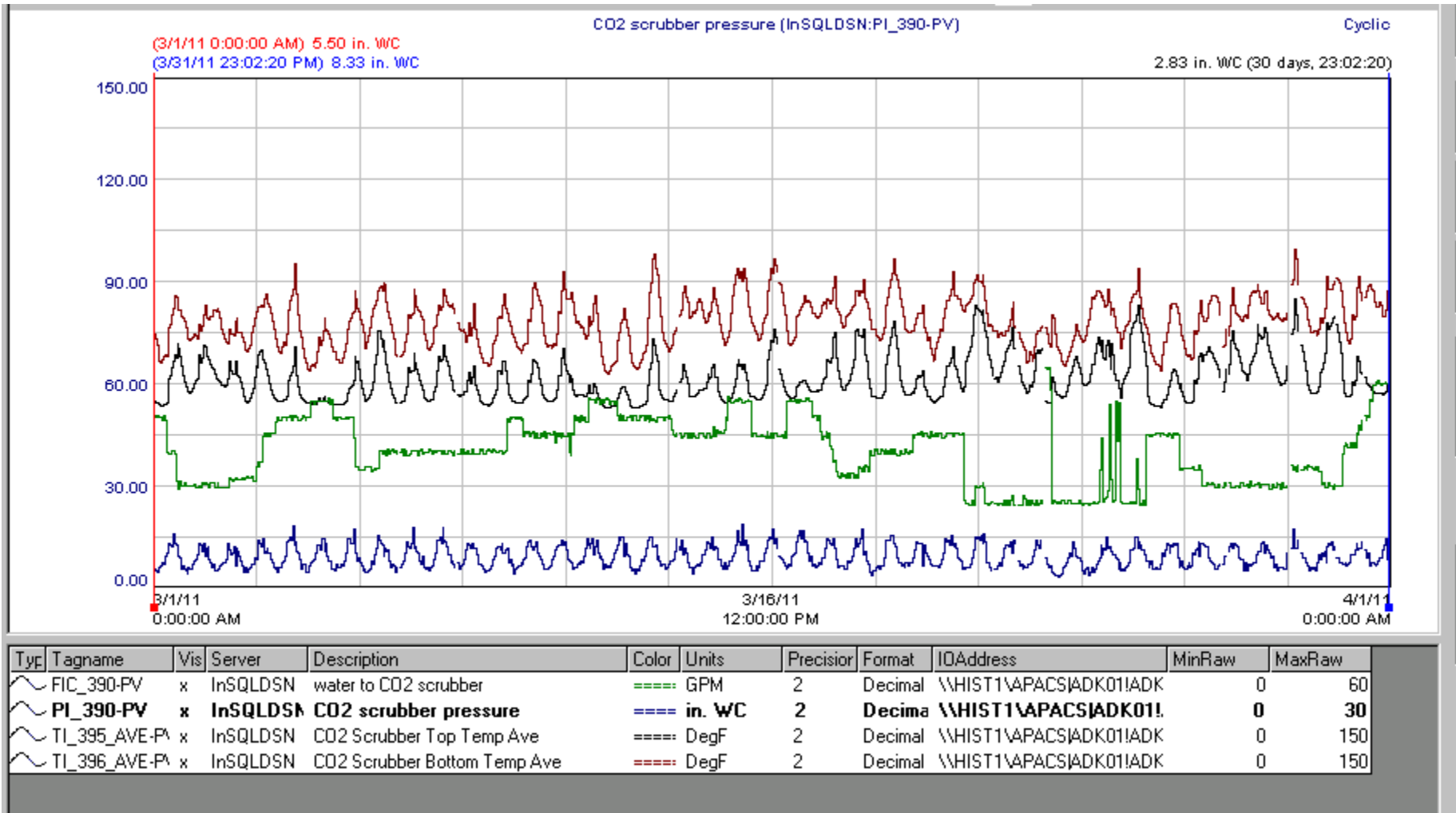
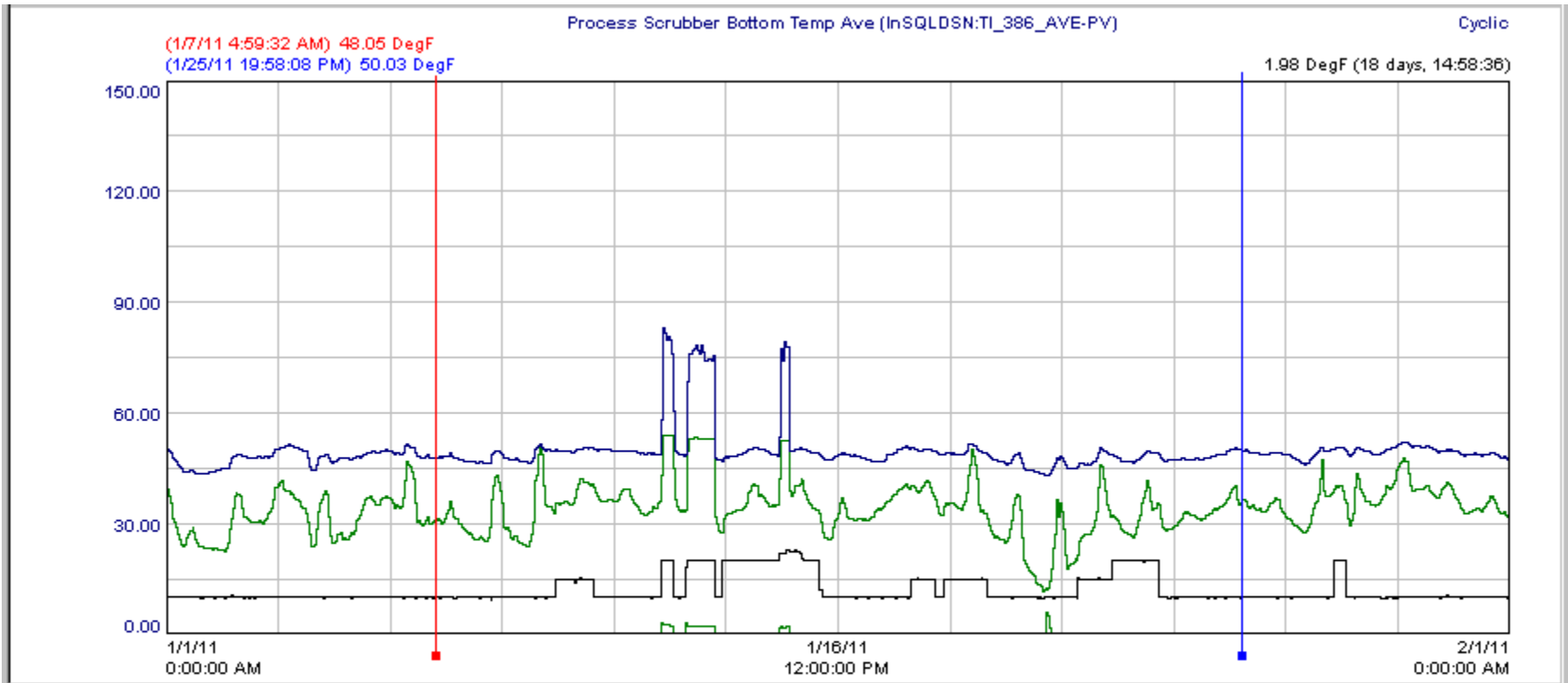


FIGURE 9

**DISTILLATION SCRUBBER TEMPERATURE
JANUARY 2011**

**Figure 9. Distillation Scrubber Temperature (cfm)
January 2011
Adkins Energy LLC – Lena, Illinois**



Typ	Tagname	Vis	Server	Description	Color	Units	Precisior	Format	IDAddress	MinRaw	MaxRaw
~	FIC_380-PV	x	InSQLDSN	water to process scrubber	=====	GPM	2	Decimal	\\HIST1\APACSIADK01\ADK	0	20
~	PI_380-PV	x	InSQLDSN	Process Scrubber	=====	in. WC	2	Decimal	\\HIST1\APACSIADK01\ADK	0	30
~	TI_385_AVE-PV	x	InSQLDSN	Process Scrubber Top Temp Ave.	=====	DegF	2	Decimal	\\HIST1\APACSIADK01\ADK	0	150
~	TI_386_AVE-PV	x	InSQLDSN	Process Scrubber Bottom Temp Ave	=====	DegF	2	Decima	\\HIST1\APACSIADK01\ADK	0	150

FIGURE 10

**DISTILLATION SCRUBBER TEMPERATURE
FEBRUARY 2011**

**Figure 10. Distillation Scrubber Temperature
February 2011
Adkins Energy LLC – Lena, Illinois**

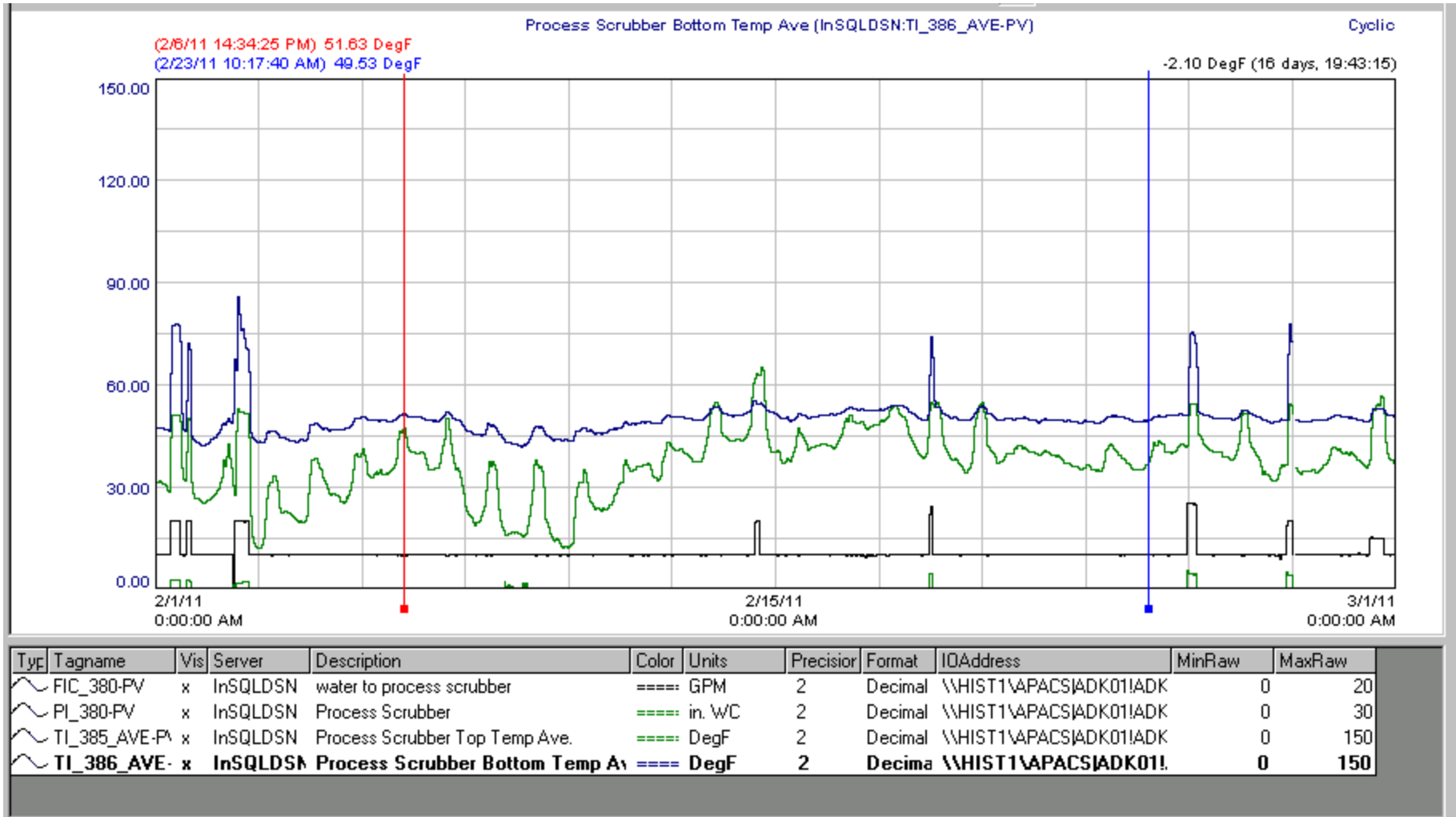


FIGURE 11

**DISTILLATION SCRUBBER TEMPERATURE
MARCH 2011**

**Figure 11. Distillation Scrubber Temperature
March 2011
Adkins Energy LLC – Lena, Illinois**

